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LIQUID PISTON GAS COMPRESSOR FOR COMPRESSED AIR ENERGY STORAGE (CAES) & CARBON DIOXIDE SEQUESTRATION

Perry Y. Li, Terry Simon, and Jim Van de Ven Kevin Nickels, Aleksander Gust and Brian Carrier

Department of Mechanical Engineering University of Minnesota

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http://www.me.umn.edu/~lixxx099/ http://www.me.umn.edu/~lixxx099/EFRI_CAES



Goals



- NSF PFI-TT Program:
 - Partnerships for Innovation: Technology Transfer
 - Program Goal: Advance previously NSF supported research towards commercialization
- Project Goal: Develop a prototype of a reciprocating high pressure (~200bar), high efficiency, liquid piston gas compressor
 - Start date: 9/1/2018



Outline



- Motivation / applications
- Challenge of isothermal gas compression/expansion
- Our approach and previous work
- Current research



Motivation:



• Grid scale energy storage as compressed air (CAES)

Carbon dioxide sequestration / reuse

Industrial gas



Grid scale energy storage

- Renewable energies abundant but also intermittent
- Requires fossil fuel powered "peaker" plants to supplement when renewables not available
- Storage can replace peaker plants
 - Increase revenue via price arbitrage
 - Stabilize electrical grid frequency
 - and







Compressed air energy storage



- Potentially cost effective for long duration (10-100hours):
 - Competition Lithium battery:
 - Cost \$270/kWh (2016), short life, rare materials.
 - Isothermal compressed air energy storage (200-350bar)
 - Engineered pressure vessels: \$40-80/kWh
 - Underground caverns: \$5/kWh
 - Energy density of "open accumulator" CAES:
 - 25kWh/m³ (210bar) and 47kWh/m³ (350bar)
 - 20 times higher than closed hydraulic accumulator at similar pressures
 - 5.5 times of conventional CAES



Open Accumulator Isothermal CAES





NSF – Emerging Frontier Research and Innovation: (2010-2016) #1038294



- High pressure, efficient and high power (fast) gas compressor/expander:
 - Key for isothermal compressed air energy storage
 - Other applications:
 - CO2 compression prior to transport for sequestration or reuse
 - Industrial gas compression:

– Linde, Praxair & Air Products together consume 1% of U.S. electricity

Challenge in Air Compression / Expansion Process

- 1. Compression :
- 2. Constant-pressure cooling :
- **3**. Expansion:

$$(P_0, T_0) \rightarrow (rP_0, T_c)$$

$$(rP_0, T_c) \rightarrow (rP_0, T_0)$$

$$(rP_0, T_0) \rightarrow (P_0, T_e)$$



Power = Work / Time



First law : $mC_v\dot{T} = -P\dot{V} - \underbrace{h\cdot A\cdot[T-T_0]}_{h\cdot A\cdot[T-T_0]}$

Q: heat transfer

Time taken:

$$t_{c/e} = \int dt = \int \frac{mC_v dT + PdV}{Q}$$

- P-V-T curve determines work and efficiency
- Heat transfer determines time
- Decreasing time increases power → lower capital cost

Adiabatic (r=350, T_0 =298K): t = 0

- Comp./expan temp: 1583K/56K
- Efficiency < 35-38%

Isothermal (T₀=298K):

• Efficiency = 100%

Target: Eff: 90-95% t =1 to 2 s







Improve heat transfer during compression/expansion process



Liquid Piston C/E with Porous Media



• Porous material \rightarrow increase surface area

- Reduce dead-volume \bullet
- Good, low friction seal
- Liquid piston trajectory controllable!

Effect of porous media (7-210 bar) : Experiments



10x increase in power density

10-15% increase in efficiency

Design of LP Compressor/Expander

- Choice and distribution
 of HX porous media
 - Heat transfer vs.
 space/cost, drag
- Choice of shape
 - Heat transfer coefficient vs liquid drag
- Choice of flow (control) trajectories
 - Efficiency vs power





Pareto Optimal Compression/ Expansion Control Problem



Given shape and porous media design, find P-V path s.t. either

- For a given efficiency (fixed work), power is maximized (minimize time); or
- 2. For a given power (time), efficiency is optimized (minimize compression work or maximize expansion work)



(* With Caleb Sancken, Andrew Rice and Mohsen Saadat)

Efficiency-Power trade-off (theoretical)



Optimal profile increases power for the same efficiency by 3 to 5 times over linear and sinusoidal profiles Increases efficiency by 15%-20%







Efficiency-Power trade-off (experimental)

> 2x power density or 5-10% increase in efficiency



Optimal Design of Compressor/Expander

- HX porous media distribution
 - Heat transfer vs. space/cost, drag, gas/liquid trapping
- Shape
 - Heat transfer coefficient. vs liquid drag and length constraint







Optimal Design Results (92%eff)





	Porosity	Flow Rate	Shape	0-D Model	
				time	Power Density
Case # 1	80% Uniform	Constant	Uniform (21.5 cm ²)	33 sec	71.2 kW/m ³
Case # 2	80% Uniform	Optimal	Uniform (21.5 cm ²)	11 sec	217.3 kW/m ³
Case # 3	80% Optimal	Constant	Uniform (21.5 cm ²)	9.6 sec	245.6 kW/m ³
Case # 4	80% Optimal	Optimal	Uniform (21.5 cm ²)	3.5 sec	669.3 kW/m ³
Case # 5	80% Optimal	Optimal	Optimal (L=69 cm)	1.6 sec	1.47 MW/m ³

Opt. Porosity: 3x improvement, as much porous media at the top Opt. Shape: 2x improvement, narrow at top

33 sec \rightarrow 1.6 sec (20 x improvement over uniform porous media)

Previous experimental compressor/expander





J. Wieberdink and B. Yan



Previous experimental system



- Emphasizes validating thermodynamic states
- Controllable flow
- Accurate measurements (pressure, volume etc.)

- Only capable of 1 compression and 1 expansion stroke
- Inefficiency liquid piston generation
- Cannot store compressed air



Current 5kW prototype design

Repeated operation:

- Reciprocating, multi-cycle
 Input-output:
- Shaft power $\leftarrow \rightarrow$ compressed air storage

Optimize cost instead of size

Challenges: Valve design; liquid piston sensing and control; dead-volume management; efficient PTO



Summary



- Isothermal gas compressor/expander have wide market potential for green economy
- Key challenge: high efficiency <u>AND</u> high power
- Previous research has shown:
 - optimized liquid piston w/ porous media C/E approach achieves
 200x increased power density at 92% efficiency
- Current research aims to create and validate a reciprocating prototype based on concept

